

# Catalytic reduction of NO<sub>2</sub> in nanocrystalline NaY zeolite

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## Abstract

In this study, in situ transmission FT-IR spectroscopy was employed to investigate the thermal and selective catalytic reduction of NO<sub>2</sub> with propylene in nanocrystalline NaY zeolite. NO was the major product in the thermal reduction of NO<sub>2</sub>. In absence of oxygen and water, selective catalytic reduction of NO<sub>2</sub> with propylene at low temperatures ( $T \leq 473$  K) resulted in the complete reduction of NO<sub>2</sub> to N<sub>2</sub> and O<sub>2</sub>. Isocyanate and nitrile species formed on extra framework alumina sites are found to be important intermediates. Based on kinetic studies, a pathway involving radical reactions appears to be the most plausible mechanism for the complete reduction of NO<sub>2</sub>. © 2004 Elsevier B.V. All rights reserved.

**Keywords:** Selective catalytic reduction; NO<sub>2</sub>; Y zeolite; Propylene; Nanoparticles

## 1. Introduction

The emission control of nitrogen oxides (NO<sub>x</sub>) from engine exhaust is of great importance due to their contribution to processes harmful to the environment [1–3]. Selective catalytic reduction (SCR) of NO<sub>x</sub> with NH<sub>3</sub> or hydrocarbons (HCs) has emerged as an effective technology using oxide and zeolite based catalysts [4–6]. Zeolites are considered particularly promising SCR catalysts because of their cation exchange capacity and acid–base properties.

Several recent studies have investigated alkali and alkaline earth-exchanged Y, FAU zeolites in the adsorption and HC-SCR of NO<sub>x</sub> [7–14]. NO<sub>2</sub> can be stored in zeolite Y in the form of stable nitrate and nitrite species. The adsorption of NO<sub>2</sub> (or NO + O<sub>2</sub>) in zeolite Y has been suggested to proceed via the disproportionation of N<sub>2</sub>O<sub>4</sub> or the reaction of NO<sub>2</sub> with the residual water in zeolite. As for the mechanism of HC-SCR, previous studies have suggested isocyanates to be key intermediates in this reaction

[15,16]. Organic nitro/nitrito compounds are first generated in the reaction between adsorbed hydrocarbons and surface nitrate/nitrite species. These compounds are then converted to isocyanates. Isocyanates will react with NO<sub>x</sub> from the gas phase producing dinitrogen. Although the general reaction scheme can be understood from these steps, many details still remain elusive, such as the mechanism for the formation of the nitrogen–nitrogen bond in complete reduction. Ammonium ions or free radicals have been proposed as key intermediates in the formation of dinitrogen [7,17].

Most HC-SCR studies in zeolites have been carried out at temperatures above 673 K. At these elevated temperatures, many side reactions can take place [3]. In this study, thermal reduction and propylene-SCR of NO<sub>2</sub> were done at lower temperatures ( $T \leq 473$  K) and monitored with in situ FT-IR spectroscopy. Infrared spectroscopy has been widely used to investigate the adsorption and the selective catalytic reduction of NO<sub>x</sub> [18–22]. In particular, information concerning the kinetics and mechanism of these reactions may be discerned from this spectroscopic technique. In addition, synthesized nanocrystalline NaY zeolite was used as the catalyst instead of commercially available zeolite catalysts. As discussed in a recent publication, nanocrystalline zeolites may be particularly useful in environmental applications due to

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the small particle size and large internal and external surface areas [23,24].

## 2. Experimental

### 2.1. Zeolite sample preparation and materials

Nanocrystalline NaY zeolite was synthesized according to methods described in the literature [25]. Two solutions (A and B) were prepared. Solution A was obtained by dissolving NaOH and tetramethylammonium hydroxide (TMAOH) in distilled water and then adding aluminum isopropylate to the alkali solution. Solution B was prepared by adding tetraethyl orthosilicate (TEOS) to the remainder of the TMAOH solution. Both solutions were filtered through a 0.2  $\mu\text{m}$  filter paper, then mixed together and stirred overnight at room temperature. The clear solution mixture obtained was then heated in a Teflon-lined stainless steel autoclave for 3 days at 403 K. The resulting solution was centrifuged for 30 min at 3400 rpm. The product was washed with distilled water and dried in air.

The synthesized zeolite was characterized using powder X-ray diffraction (Siemens D5000) to assess the crystallinity and to verify the identity of the zeolite. Scanning electron microscopy (SEM, Hitachi S-4000) was used to determine particle morphology and particle size. The average particle size was determined to be  $80 \pm 30$  nm from SEM. The surface area was measured on an automated Quantachrome Nova 1200 multipoint BET apparatus. The internal and external surface areas of the synthesized zeolite were 474 and  $46 \text{ m}^2 \text{ g}^{-1}$ , respectively. Based on previous work [26], the particle size of the zeolite was calculated using the external surface area to be approximately 88 nm, in reasonable agreement with the SEM measurement.  $^{27}\text{Al}$  and  $^{29}\text{Si}$  magic angle spinning (MAS) NMR (300 MHz wide bore, Tecmag) were performed on the sample. NMR signals from tetrahedral Al and Si atoms were identified. The Si/Al ratio was determined to be 1.7 from  $^{29}\text{Si}$  MAS NMR.

Research-grade purity oxygen and carbon dioxide were purchased from Air Products. Research-grade purity nitrogen dioxide, propylene, nitric oxide, nitrous oxide and carbon monoxide from Matheson. All gases were used as received. Pyridine (99.9%) was purchased from Fisher Scientific. Pyridine was further dehydrated over molecular sieves and purified before use by several freeze-pump-thaw cycles.

### 2.2. Fourier transform infrared spectroscopy

The infrared sample cell used in this study has been described previously [27]. Approximately 8 mg of NaY zeolite mixed with some water were coated onto a  $3 \text{ cm} \times 2 \text{ cm}$  photoetched tungsten grid held in place by nickel jaws. The nickel jaws are attached to copper leads so that the sample can be resistively heated. A thermocouple wire attached to the tungsten grid is used to measure the temperature of the

sample. The tungsten grid with zeolite sample is placed inside of a stainless steel cube. The cube has two  $\text{BaF}_2$  windows for infrared measurements and is connected to a vacuum/gas handling system.

The stainless steel IR cell is held in place by a linear translator inside the sample compartment of a Mattson Galaxy 6000 infrared spectrometer equipped with a narrow-band MCT detector. The linear translator allows each half of the sample grid to be translated into the infrared beam. This permits the detection of gas phase and adsorbed species in zeolites under identical reaction conditions. Each spectrum was obtained by averaging 64 scans at an instrument resolution of  $4 \text{ cm}^{-1}$ . Each absorbance spectrum shown represents a single beam scan referenced to the appropriate single beam scan of the clean zeolites or the blank grid, unless otherwise noted.

The NaY sample was gradually heated under vacuum at 573 K or higher temperature overnight to remove adsorbed water. Reactant gases were loaded into the zeolite through the gas handling system. Two absolute pressure transducers were used to monitor the pressures. Typically, the zeolite was equilibrated with each gas prior to a spectrum being recorded. In pyridine adsorption experiments, adsorption was carried out by equilibrating the zeolite powder with 1 Torr pressure of pyridine vapor at room temperatures. The sample was then evacuated for 30 min before a spectrum was recorded. The desorption of pyridine was monitored by evacuating the sample for 30 min at elevated temperatures and cooling back to room temperature prior to recording a spectrum.

In SCR reactions,  $\text{NO}_2$  and propylene (1:1 ratio) were pre-mixed in a chamber before being introduced into the IR cell at room temperature. Time course experiments were conducted by automatically scanning the gas phase every 2 min. The extinction coefficient of individual gases was calibrated using the characteristic IR absorption bands and measuring the pressure using an absolute pressure transducer. Assuming ideal gas behavior, the amount of gas can be calculated from its pressure and volume of the IR cell.

## 3. Results

### 3.1. An investigation of the nature of the surface sites on nanocrystalline NaY

Five absorption bands due to hydroxyl groups were identified in the infrared spectra after heating the NaY zeolite overnight under vacuum at temperatures of 573 and 673 K, as shown in Fig. 1. Although there is an overall decrease in intensity of the band in this region after heating from 573 to 673 K, the five absorption bands are still evident at 673 K. The relatively intense high frequency absorption band at  $3745 \text{ cm}^{-1}$  is assigned to terminal silanol groups that are on the external surface of the particles. This feature is of much weaker intensity in a commercial sample of NaY zeolite that has a much larger particle size [23]. Thus, this result

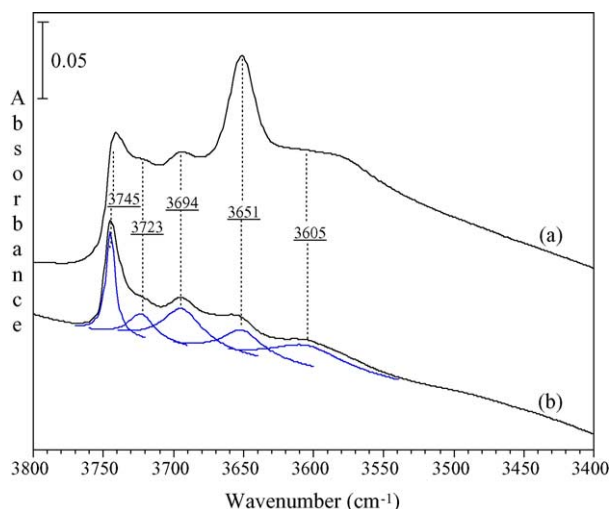


Fig. 1. FT-IR spectra of surface hydroxyl groups in nanocrystalline NaY zeolite after heating to (a) 573 K and (b) 673 K overnight under vacuum. The two spectra were recorded at  $T=298$  K. Five different O–H groups were identified in the spectrum. The spectrum recorded after heating to 673 K overnight is fit to five bands with Lorentzian line-shapes so that these bands can be more readily discerned. The blank grid is used as a reference.

confirms that the synthesized NaY zeolite consists of small particles. The next highest frequency absorption band around  $3723\text{ cm}^{-1}$  is associated with hydroxyl groups occurring at defect sites (also called hydroxyl nests) [28]. The absorption band at  $3694\text{ cm}^{-1}$  has been assigned to surface hydroxyl groups near  $\text{Na}^+$  sites, while the bands at  $3654$  and  $3605\text{ cm}^{-1}$  are associated with hydroxyl group attached to extra framework alumina (EFAL) species [29,30] and adsorbed water, respectively.

Several probe molecules were used to detect the presence of additional surface adsorption sites for the synthesized nanocrystalline zeolite Y used in this study. The adsorption of propylene in NaY (see Fig. 2) results in an absorption band at  $1635\text{ cm}^{-1}$  assigned to the C=C stretching mode and several bands between  $1350$  and  $1500\text{ cm}^{-1}$  associated with the  $\text{CH}_3$  deformation mode and the  $\text{CH}_2$  scissor mode. Absorptions due to C–H stretching modes between  $2800$  and  $3100\text{ cm}^{-1}$  were also observed (not shown). All of the absorption features disappeared after evacuation of gas-phase propylene at room temperature for several minutes. With excess propylene in the IR cell, no pronounced change of the band at  $1635\text{ cm}^{-1}$  was observed at room temperature for 6 h, indicating that propylene did not undergo polymerization in the nanocrystalline NaY zeolite. It can therefore be concluded that strong Bronsted acid sites that initiate propylene polymerization are not present in the nanocrystalline NaY zeolite pretreated at 573 K [31]. The FT-IR spectra shown in Fig. 1 are consistent with this conclusion as strong Bronsted acid sites are typically bridging OH groups with vibrational frequencies of  $3630$  and  $3560\text{ cm}^{-1}$  [29,32]. These bands are not observed in the infrared spectra of nanocrystalline NaY shown in Fig. 1.

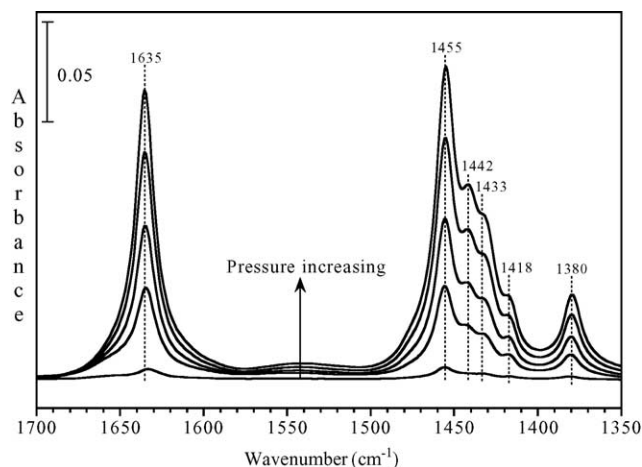


Fig. 2. FT-IR spectra of propylene adsorbed in nanocrystalline NaY zeolite at  $T=298$  K as a function of propylene pressure ( $P=0.050, 0.493, 1.019, 2.028$  and  $4.061$  Torr). All spectra shown in Fig. 2 use the clean nanocrystalline NaY zeolite prior to adsorption as a reference. In addition, gas-phase absorptions have been subtracted from each of the FT-IR spectra.

Pyridine adsorption, however, revealed the existence of weaker Bronsted acid sites as well as Lewis acid sites in the NaY zeolite. It is well known that weakly adsorbed pyridine with characteristic vibrational frequencies of  $1617, 1592, 1574$  and  $1441\text{ cm}^{-1}$  desorbs near  $470\text{ K}$  [32,33]. In contrast, pyridinium ions with characteristic vibrational frequencies of  $1632$  and  $1545\text{ cm}^{-1}$  generated by reaction with Bronsted acid sites desorb at much higher temperatures. Similarly, pyridine molecules that adsorbed at Lewis acid sites are also more strongly adsorbed. Pyridine molecules adsorbed at Lewis acid sites can be identified from characteristic absorptions at  $1621$  and  $1454\text{ cm}^{-1}$ . All three types of adsorbed pyridine molecules contribute to the absorption band at  $1489\text{ cm}^{-1}$ . Fig. 3 displays the FT-IR spectra of pyridine molecules adsorbed in the nanocrystalline NaY zeolite following desorption at three different temperatures ( $298, 373$  and  $473\text{ K}$ ). It can be seen from the infrared spectrum at  $298\text{ K}$  that all three types of adsorbed pyridine molecules are observed. After heating to higher temperatures, only pyridine molecules adsorbed on Bronsted and Lewis acid sites are apparent in the infrared spectra. The Bronsted acid sites may be associated with the surface hydroxyl groups attached to EFAL species.

### 3.2. Adsorption and thermal reduction of $\text{NO}_2$

The adsorption and reaction of  $\text{NO}_2$  on surfaces have been extensively studied due to its environmental importance. FT-IR spectra recorded of the NaY zeolite as a function of  $\text{NO}_2$  pressure are shown in Fig. 4. It is evident from the spectra that exposure to  $\text{NO}_2$  results in the formation of several surface species whose frequencies fall into two spectral regions:  $1200$ – $1660\text{ cm}^{-1}$  due to  $\text{NO}_3^-$  and  $\text{NO}_2^-$   $1900$ – $2300\text{ cm}^{-1}$  due to  $\text{NO}^+$ . Previous studies on nitrogen oxide adsorption make the assignment of the spectra relatively straightforward [34–39]. At low pressures, a doublet with absorbance max-

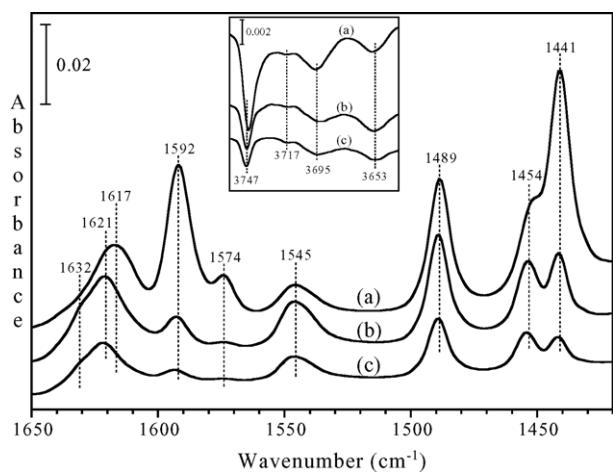


Fig. 3. FT-IR spectra of pyridine molecules adsorbed in nanocrystalline NaY zeolite at  $T=298$  K following pyridine desorption at (a) 298 K, (b) 473 K and (c) 573 K. The inset shows the spectral region extending from 3635 to 3760  $\text{cm}^{-1}$ . The spectra were recorded at 298 K. All spectra shown in Fig. 3 use the clean nanocrystalline NaY zeolite prior to adsorption as a reference. In addition, gas-phase absorptions have been subtracted from each of the FT-IR spectra. The peaks in the spectra are assigned to weakly adsorbed pyridine and pyridine adsorbed on acid sites. See text for further details.

ima at 1410 and 1386  $\text{cm}^{-1}$  can be attributed to the  $\nu_3$  mode splitting of surface nitrate ( $\text{NO}_3^-$ ) adsorbed on  $\text{Na}^+$  sites. At higher loading, the doublet converges into a singlet with a frequency of 1407  $\text{cm}^{-1}$ . This broadening of the nitrate bands is most likely due to intermolecular interactions [11,12]. The absorption at 1230  $\text{cm}^{-1}$  is associated with adsorbed nitrite ( $\text{NO}_2^-$ ). Absorption bands at 1627, 1581 and 1554  $\text{cm}^{-1}$  are associated with nitrate absorptions on the EFAL bonded in different coordinations (bridging, bidentate and monodentate, respectively) [2]. The absorption at 1327  $\text{cm}^{-1}$  is also associated with nitrate adsorption on EFAL sites.

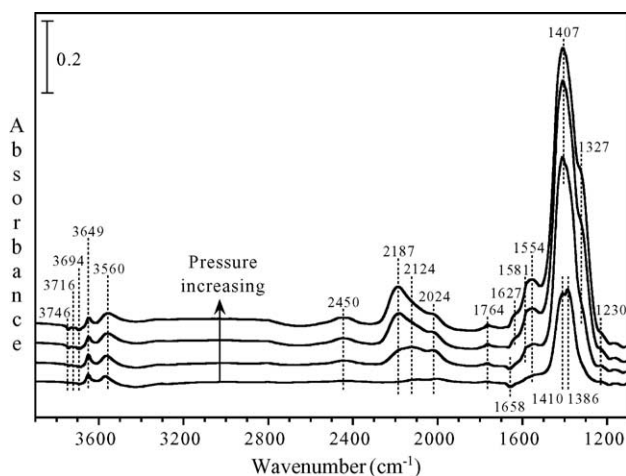


Fig. 4. FT-IR spectra of  $\text{NO}_2$  adsorbed in nanocrystalline NaY zeolite at  $T=298$  K as a function of  $\text{NO}_2$  pressure ( $P=0.055, 0.107, 0.498$  and  $1.033$  Torr). All spectra shown in Fig. 4 use the nanocrystalline NaY zeolite prior to adsorption as a reference. In addition, gas-phase absorptions have been subtracted from each of the FT-IR spectra.

The absorption bands within the spectral region between 1900 and 2300  $\text{cm}^{-1}$  are assigned to nitrosonium ions ( $\text{NO}^+$ ) [11,40]. At low pressures, two bands at 2024 and 2124  $\text{cm}^{-1}$  are due to the formation of  $\text{NO}^+$  species adsorbed onto different cationic position in the zeolite framework. At high pressures, an absorption feature at 2187  $\text{cm}^{-1}$  develops. This feature can be assigned to the N–O stretching mode from  $[\text{NO}^+][\text{NO}_2]$  or  $[\text{NO}^+][\text{N}_2\text{O}_4]$  adducts adsorbed onto Lewis base sites [11,12]. Two other bands at 2450 and 1764  $\text{cm}^{-1}$  can be assigned to an overtone and combination bands of adsorbed nitrates [22].

In the hydroxyl group region, loss of three bands at 3694, 3716 and 3746  $\text{cm}^{-1}$  was observed because of either the displacement or interaction of hydroxyl groups with adsorbed  $\text{NO}_x^-$  species. Perturbed hydroxyl groups on EFAL species gave rise to two absorptions at 3649 and 3560  $\text{cm}^{-1}$  [12]. At low  $\text{NO}_2$  pressure, a negative peak around 1658  $\text{cm}^{-1}$  was visible, indicating the consumption of residual  $\text{H}_2\text{O}$  in the zeolite upon  $\text{NO}_2$  adsorption.

Thermal reduction of  $\text{NO}_2$  at temperatures from 298 to 573 K was investigated. FT-IR spectra of the gas phase were taken at 2 min time intervals. The concentration of the gases in the infrared cell can be determined from the integrated absorbances of the bands at 1616  $\text{cm}^{-1}$  ( $\text{NO}_2$ ), 1875  $\text{cm}^{-1}$  ( $\text{NO}$ ) and 2224  $\text{cm}^{-1}$  ( $\text{N}_2\text{O}$ ) using calibrated extinction coefficients. The time course concentration of gas-phase products in thermal reduction of  $\text{NO}_2$  at 373 K is shown in Fig. 5. Immediately after heating began, the concentration of  $\text{NO}_2$  in the gas phase jumped to a maximum and then decreased quickly. Clearly a large amount of  $\text{NO}_2$  was released from the NaY zeolite upon heating, possibly via the reaction of highly active surface nitrate [41].  $\text{NO}$  and  $\text{N}_2\text{O}$  were the only other gas-phase products detected by the FT-IR spectroscopy.

The product distribution and conversion of both gaseous  $\text{NO}_2$  and adsorbed  $\text{NO}_3^-$  at three different temperatures are listed in Table 1. In thermal reduction of  $\text{NO}_2$ ,  $\text{NO}$  was the major product.  $\text{N}_2\text{O}$  accounted for less than 2% of the prod-

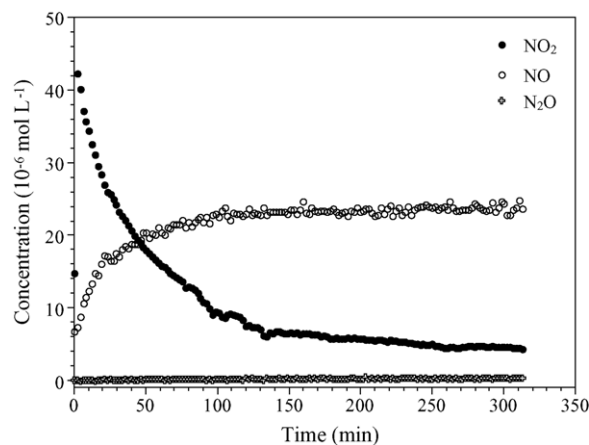


Fig. 5. Time evolution of gas phase  $\text{NO}_2$ ,  $\text{NO}$  and  $\text{N}_2\text{O}$  during the thermal reduction of  $\text{NO}_2$  in nanocrystalline NaY at 373 K. Spectra were recorded every 2 min.

Table 1  
Product distribution and conversion of gas-phase  $\text{NO}_2$  and adsorbed  $\text{NO}_3^-$  in the thermal reduction of  $\text{NO}_2$  at different temperatures after 6 h of reaction time

Reaction temperature (K)	Gas products ( $\mu\text{mol L}^{-1}$ ) <sup>a</sup>		% Conversion <sup>b</sup>	
	NO	$\text{N}_2\text{O}$	$\text{NO}_2$	$\text{NO}_3^-$
298	10.1	0	79	11
373	23.6	0.2	71	64
473	51.3	0.8	92	90

<sup>a</sup> In thermal reduction, the total loading of  $\text{NO}_2$  was controlled to be  $50 \pm 5 \mu\text{mol L}^{-1}$ ; the initial concentration of gas-phase  $\text{NO}_2$  after adsorption equilibrium at 298 K was  $14 \pm 2 \mu\text{mol L}^{-1}$ .

<sup>b</sup> Conversion of  $\text{NO}_2$  refers to change of  $\text{NO}_2$  in gas phase; conversion of  $\text{NO}_3^-$  describes the change associated with the integrated absorbance in the entire 1240–1660  $\text{cm}^{-1}$  spectral region.

ucts in the temperature range studied. More than 70% of gas-phase  $\text{NO}_2$  decomposed after reaction at 373 K for 6 h. The efficiency reached 100% when the temperature was above 523 K. The concentration of  $\text{N}_2$  and  $\text{O}_2$  couldn't be monitored in this study. However, based on the nitrogen mass balance, it appears that little  $\text{N}_2$  and  $\text{O}_2$  were formed in the thermal reduction of  $\text{NO}_2$ .

In order to measure the thermal stability of the various surface species in the zeolite,  $\text{NO}_2$  was first adsorbed in nanocrystalline NaY zeolite at 298 K and the sample was then heated to different temperatures. Fig. 6 shows the FT-IR spectra of surface species adsorbed in NaY zeolite after evacuating the zeolite at different temperatures. Surface adsorbed  $\text{NO}^+$  was removed completely by evacuating at 298 K for 30 min, while less than 10% of the original  $\text{NO}_3^-$  species still remained adsorbed in the zeolite after heating to 573 K. The quantitative study by Sedlmair et al. has shown the relative stability of the  $\text{NO}_x$  surface species as following:  $\text{Na}^+$ -

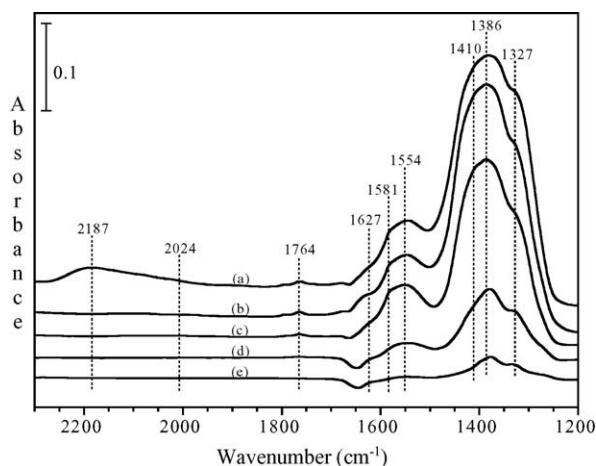


Fig. 6. FT-IR spectra of  $\text{NO}_2$  adsorbed in nanocrystalline NaY zeolite after adsorption at (a) 298 K in the presence of the gas phase and (b) after evacuation of the gas phase. The sample was then heated to (c) 373 K, (d) 473 K and (e) 573 K for 30 min. All spectra were recorded at  $T = 298$  K. All spectra shown in Fig. 6 use the nanocrystalline NaY zeolite prior to adsorption as a reference. In addition, gas-phase absorptions have been subtracted from each of the FT-IR spectra.

Table 2  
Assignment of infrared absorption bands observed following adsorption of  $\text{NO}_2$  and propylene (1:1) mixture in nanocrystalline NaY zeolite

Bands ( $\text{cm}^{-1}$ )	Assignments	Possible species	Reference
3300–3150	$\nu(\text{OH})$	Oximes	[18,47]
2985	$\nu(=\text{CH}_2)$	$\text{RCH}=\text{CH}_2$	[42]
2317	$\nu(\text{NCO})$	$\text{SiNCO}$	[43,44]
2272	$\nu(\text{NCO})$	$\text{HNCO}$	[7,44]
2239	$\nu(\text{NCO})$	$\text{RNCO}$	[19,48–52]
2187	$\nu(\text{CN})$	$\text{RCN}$	[48,51,52]
1969	$\nu(\text{N}=\text{O})$	$\text{NO}$ (a)	[35]
1943	$\nu(\text{N}=\text{O})$	$\text{N}_2\text{O}_3$ (a)	[35]
1723, 1694	$\nu(\text{C}=\text{O})$	Carbonyl species	[7,47]
1647	$\nu(\text{ONO})$	$\text{RONO}$ (or $\text{RCONH}_2$ )	[7,20,21,47]
1598, 1483	–	Carbonaceous species	[46]
1557, 1387	$\nu(\text{NO}_2)$	$\text{RNO}_2$	[7,20,21,47]
1528	$\nu(\text{CO}_3^{2-})$	Carbonate ion	[42]
1508	$\nu(\text{COO}^-)$	Formate ion	[42]
1354	$\delta(\text{CH}_3)$	$\text{RCH}_3$	[7]
1282	$\nu(\text{C}=\text{O})$	$\text{RONO}$	[45]

nitrate > Al-nitrate > nitrite [12]. In our work, nitrates also appear to be the more stable species relative to nitrites and nitrosonium ions.

### 3.3. Adsorption of $\text{NO}_2$ and propylene (1:1) mixture

In the propylene-SCR reaction,  $\text{NO}_2$  and propylene were pre-mixed (1:1 mole ratio) in a chamber prior to being introduced into the infrared cell. The FT-IR spectra of the resulting mixture adsorbed in NaY zeolite at 298 K are shown in Fig. 7. In comparison to the adsorption of  $\text{NO}_2$  alone, similar absorption features were observed in the  $\text{NO}_3^-$  region. In addition, several new absorption bands were also observed. Assignments of these bands are given in Table 2. Most of

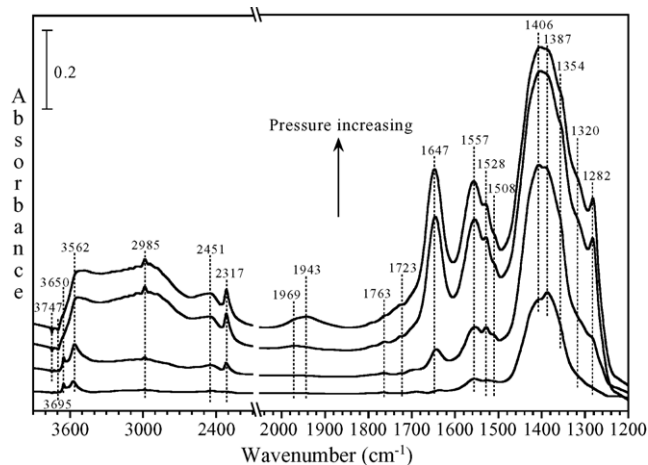


Fig. 7. FT-IR spectra of  $\text{NO}_2$  and propylene (1:1) mixture adsorbed in nanocrystalline NaY zeolite at 298 K recorded as a function of increasing total pressure ( $P = 0.100, 0.200, 0.623, 1.005$  Torr). All spectra shown in Fig. 7 use the nanocrystalline NaY zeolite prior to adsorption as a reference. In addition, gas-phase absorptions have been subtracted from each of the FT-IR spectra.

these assignments are based on previous studies reported in the literature [42–52].

It is important to note that the spectra contain a wealth of information and there is some considerable overlap of some of the bands in several spectral regions. For example, both  $\text{Na}^+$ -nitrates and surface adsorbed organic nitro compounds can contribute to the intensity of the observed band at  $1387\text{ cm}^{-1}$ . The absorption at  $1647\text{ cm}^{-1}$  is assigned to organic nitrito species, but it may also, in part, be due to the formation of carbonyl groups in primary amides or the  $\text{C}=\text{N}$  stretching mode of oximes [47,48]. Therefore, careful analysis of the FT-IR spectra is important in identifying the adsorbates present. Thermal stability of the surface compounds was investigated to assist in making these spectral assignments. The NaY zeolite was equilibrated with  $\text{NO}_2$  and propylene (1:1) mixture for 30 min. After evacuating the gas phase, the NaY zeolite was heated for 30 min and cooled back to room temperature before recording each of the spectra shown in Fig. 8.

Adsorption of the  $\text{NO}_2$  and propylene mixture results in the formation of several oxygenated and nitrogen-containing organic compounds. As seen in Figs. 7 and 8, adsorbed oxygenated hydrocarbons ( $\text{C}_x\text{H}_y\text{O}_z$ ) with absorptions at 2985, 1723, 1694, 1528, 1508 and  $1354\text{ cm}^{-1}$  appear immediately in the spectrum recorded at 298 K. Carbonyl group containing compounds may come about from the direct oxidation of adsorbed propylene by adsorbed  $\text{NO}_x^-$  [22,41,53]. Two bands at 1528 and  $1508\text{ cm}^{-1}$  develop quickly after the co-adsorption of  $\text{NO}_2$  and propylene. These have been previously assigned to carbenium ions formed upon adsorption of olefins on acidic zeolites [54]. Since there are no strong Bronsted acid sites in the nanocrystalline NaY zeolite used in our study, these two bands are most likely due to the formation of monodentate carbonate and formate ions, respectively [55].

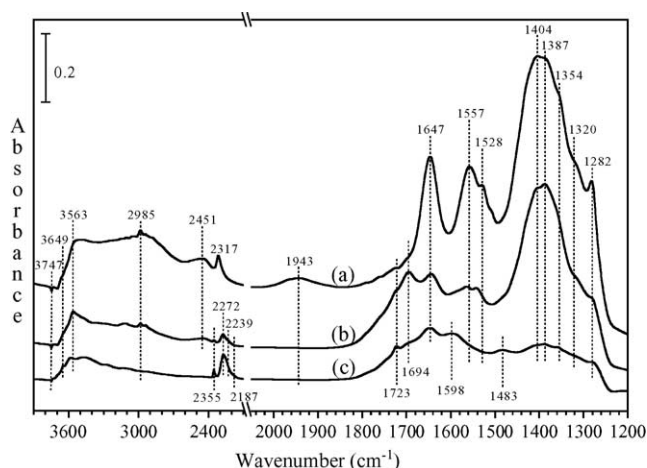


Fig. 8. FT-IR spectra of adsorbed species following adsorption of an  $\text{NO}_2$  and propylene (1:1) mixture at (a) 298 K and heating to (b) 373 K and (c) 473 K. All spectra shown in Figs. 8 use the nanocrystalline NaY zeolite prior to adsorption as a reference. In addition, gas-phase absorptions have been subtracted from each of the FT-IR spectra.

These organic compounds may be intermediates or possibly final products in the SCR reaction.

Surface adsorbed  $\text{NO}$  ( $1969\text{ cm}^{-1}$ ) and  $\text{N}_2\text{O}_3$  ( $1943\text{ cm}^{-1}$ ) appear upon adsorption of the  $\text{NO}_2$  and propylene mixture. These species are stable up to hours at room temperature. However, they disappeared quickly upon heating to 373 K. Another surface species that appears to have similar stability is identified as NCO species on  $\text{Si}^{4+}$  sites. NCO is identified by the absorption band at  $2317\text{ cm}^{-1}$  and has been identified in previous studies using isotope labels [7]. Two surface species characterized by fairly intense absorption bands at 1557 and  $1647\text{ cm}^{-1}$  appear to be more thermally stable than  $\text{NO}$ ,  $\text{N}_2\text{O}_3$  and NCO as these bands persist in the spectra even after heating to 373 K. Yeom et al. investigated the adsorption and reactions of nitromethane in zeolite Y [7]. Based on their isotopic studies, the two intense absorption bands are assigned to organic nitro ( $1557\text{ cm}^{-1}$ ) and nitrito ( $1647\text{ cm}^{-1}$ ) compounds, respectively. Another possible stable intermediate that some consider to be important in the SCR reaction is oxime. Oxime may be responsible for the broad absorbance between 3150 and  $3300\text{ cm}^{-1}$  [18].

Most of the absorption bands decreased in intensity after the nanocrystalline NaY zeolite was heated at elevated temperature. Ketones or aldehydes are produced at 373 K as indicated by the band at  $1694\text{ cm}^{-1}$  but then convert into other products by heating to 473 K. Surface adsorbed carbon dioxide ( $2355\text{ cm}^{-1}$ ) and isocyanic acid ( $2272\text{ cm}^{-1}$ ) [7] develop in the zeolite upon heating to 373 and 473 K (Fig. 8). At elevated temperature, two other absorption peaks appear in the spectra at 2239 and  $2187\text{ cm}^{-1}$  (Fig. 8). These two features have been assigned to organic isocyanate and nitrile in several previous studies using alumina-supported materials as SCR catalysts [19,48–52]. The assignments of isocyanate and nitrile have been supported by other experiments involving  $\text{NO} + \text{CO}$  reactions [50]. Since there is EFAL detected in the nanocrystalline NaY zeolite used in our study, these two absorptions are assigned to organic isocyanate and nitrile adsorbed on EFAL sites. They most likely come from the thermal reaction of organic nitro/nitrito compounds or oxime. Unlike the band at  $1557\text{ cm}^{-1}$ , the absorption at  $1647\text{ cm}^{-1}$  persists even after heating to 473 K. This may indicate the formation of a primary amide, which can be generated via the hydrolysis of nitriles and/or thermal reaction of organic nitro/nitrito species. The assignment for the bands at 1598 and  $1483\text{ cm}^{-1}$  is difficult since there are numerous literature assignments for bands at these two frequencies and are most likely due to the presence of unsaturated carbonaceous residues or coke [46]. Organic isocyanates and coke are the only compounds adsorbed in NaY zeolite after evacuating the sample overnight at 673 K.

### 3.4. Low temperature propylene-SCR of $\text{NO}_2$

Propylene-SCR of  $\text{NO}_2$  at different temperatures was investigated next. The FT-IR spectra of the gas phase as a func-

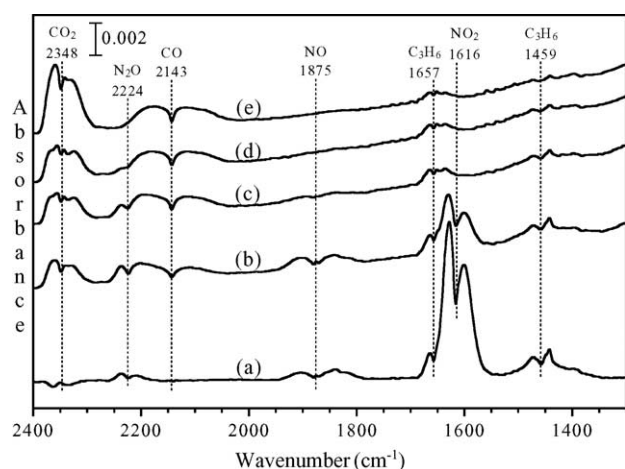


Fig. 9. FT-IR spectra of the gas phase following propylene-SCR of  $\text{NO}_2$  in nanocrystalline NaY at 473 K for (a) 0 min, (b) 10 min, (c) 30 min, (d) 1 h and (e) 4 h.

tion of time at a temperature of 473 K is shown in Fig. 9. The concentration of the gases was again calculated from the integrated absorbance of the individual band using the calibration procedure discussed in the experimental section. Fig. 10 shows the amount of the various gaseous species as a function of time in propylene-SCR of  $\text{NO}_2$  at 473 K. Immediately after the heating process begins, gaseous  $\text{NO}_2$  decreases and is completely gone after 25 min. The concentrations of NO and  $\text{N}_2\text{O}$  initially increase until a maximum is reached at approximately  $t = 10$  min, then gradually decrease to zero. Propylene ( $1459$  and  $1657$   $\text{cm}^{-1}$ ), CO ( $2143$   $\text{cm}^{-1}$ ) and  $\text{CO}_2$  ( $2348$   $\text{cm}^{-1}$ ) were the only carbon-containing molecules detected in the gas phase. Although not directly measured,  $\text{N}_2$  and  $\text{O}_2$  most likely form as well, based on the estimated nitrogen mass balance. Some water is apparent in the gas-phase spectra as well. A similar time course experiment was done at  $T = 373$  K. These data are summarized in Table 3 with some additional experiments as well.

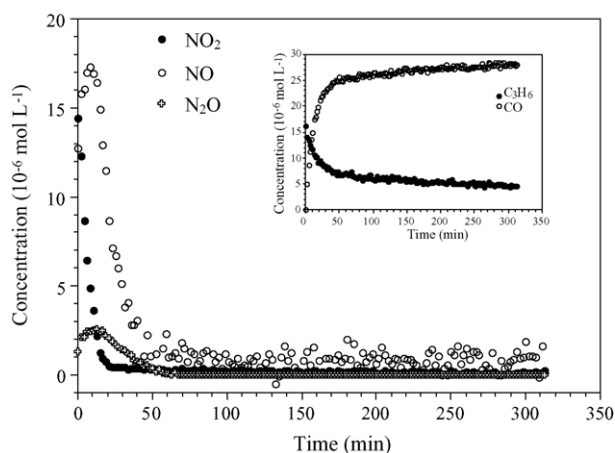


Fig. 10. Evolution of gaseous N-containing species during propylene-SCR of  $\text{NO}_2$  in nanocrystalline NaY at 473 K. The inset shows the decay and evolution of propylene and carbon monoxide, respectively. Spectra were recorded every 2 min.

Table 3  
Product distribution and conversion of gas-phase  $\text{NO}_2$  and adsorbed  $\text{NO}_3^-$  in propylene-SCR of  $\text{NO}_2$  at different temperatures after 6 h of reaction time

Reaction temperature (K)	Product distribution ( $\mu\text{mol L}^{-1}$ ) <sup>a</sup>				%Conversion <sup>b</sup>	
	NO	$\text{N}_2\text{O}$	CO	$\text{CO}_2$	$\text{NO}_2$	$\text{NO}_3^-$
298	12.5	3.0	0	0	82	0
373	0	0.4	24.7	1.6	100	3
473	0	0	28.1	8.6	100	29
473 <sup>c</sup>	40.9	3.7	6.4	13.9	100	68
473, $\text{O}_2$ <sup>d</sup>	25.1	4.6	1.3	40.7	100	87

<sup>a</sup> The total loading of  $\text{NO}_2$  was  $50 \pm 5$   $\mu\text{mol L}^{-1}$ ; in the absence of oxygen the initial concentration of gas-phase  $\text{NO}_2$  after adsorption equilibrium at 298 K was  $16 \pm 4$   $\mu\text{mol L}^{-1}$ .

<sup>b</sup> Conversion of  $\text{NO}_2$  refers to the change of  $\text{NO}_2$  in gas phase; conversion of  $\text{NO}_3^-$  describes the change associated with the integrated absorbance in the entire  $1230$ – $1600$   $\text{cm}^{-1}$  spectral region (because of overlapping absorption bands due to other adsorbed species, this estimate could be in error by as much as 20%).

<sup>c</sup> Propylene-SCR of  $\text{NO}_2$  was done using a partially deactivated zeolite catalyst (see text for further details).

<sup>d</sup> Propylene-SCR of  $\text{NO}_2$  with  $\text{O}_2$  present in the IR cell.

Table 3 summarizes the gas-phase product distribution and percent conversion of gas-phase  $\text{NO}_2$  and adsorbed nitrate (vide infra) in propylene-SCR of  $\text{NO}_2$  at three different temperatures (298, 373 and 473 K). Based on the nitrogen balance, the complete reduction of  $\text{NO}_2$  into  $\text{N}_2$  and  $\text{O}_2$  was found at 473 K after 6 h of reaction. Although a small amount of  $\text{N}_2\text{O}$  existed after 6 h at 373 K, it was expected that it too would disappear with longer reaction time. CO and  $\text{CO}_2$  were generated as the major carbon containing products in the gas phase.

It should be pointed out that the conversion of  $\text{NO}_3^-$  in Table 3 stands for the conversion of species responsible for the absorption bands between  $1230$  and  $1600$   $\text{cm}^{-1}$ . Even though some of the absorptions in the region are due to other adsorbates, it can still be an approximate measure of how much  $\text{NO}_3^-$  species reacted since  $\text{NO}_3^-$  accounts for most of the absorbance in that region (estimated to be  $\sim 90\%$ ).

Complete conversion of  $\text{NO}_2$  did not occur when coke accumulated in the NaY zeolite (referred to as “partially deactivated NaY zeolite” in Table 3). Propylene-SCR of  $\text{NO}_2$  at 473 K in a partially deactivated NaY zeolite converted approximately 90% of loaded  $\text{NO}_2$  into NO and  $\text{N}_2\text{O}$ . The evolution of  $\text{NO}_2$ , NO and  $\text{N}_2\text{O}$  with time was similar to that of thermal reduction, except for the higher concentration of  $\text{N}_2\text{O}$ . Compared to SCR reaction in active NaY zeolite, less propylene was consumed, but the  $\text{CO}_2$  to CO ratio and conversion of  $\text{NO}_3^-$  were much higher. More undesired products, i.e. partially oxidized organics, were generated in the zeolite as well. These products include surface adsorbed carbonyl compounds ( $1723$  and  $1694$   $\text{cm}^{-1}$ ).

Although an excess amount of oxygen is present under typical lean burn conditions, only propylene and  $\text{NO}_2$  were included in the starting reaction mixture in this study for several reasons. First, an intermediacy of  $\text{NO}_2$  in SCR of propylene has been suggested [6]. Furthermore, the oxidation of propylene

Table 4  
Initial reaction rates ( $10^{-2} \mu\text{mol L}^{-1} \text{s}^{-1}$ ) in first 10 min

Reaction temperature (K)	Thermal (NO)	Propylene-SCR		
		NO <sub>2</sub> (loss)	PE (loss)	CO
298	0.1	0.4	0	0
373	1.0	2.1	0.7	2.9
473	2.8	2.0	0.8	2.6
473 <sup>a</sup>		0.9	0.3	0.4

<sup>a</sup> Propylene-SCR of NO<sub>2</sub> was done using a partially deactivated zeolite catalyst (see text for further details).

by oxygen competes with the SCR reaction. This is confirmed by the propylene-SCR of NO<sub>2</sub> in nanocrystalline NaY zeolite at 473 K in the presence of oxygen, propylene was found to be consumed within 2 h at 473 K. The concentration of NO reached a maximum and then decreased slowly.

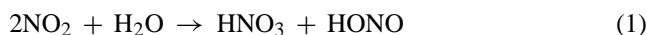
Table 4 summarizes the initial reaction rates in catalytic reduction of NO<sub>2</sub>. The initial reaction rates were obtained by linear fitting the concentration of individual gaseous species in the first 10 min of the reaction. NO for thermal reduction, NO<sub>2</sub>, propylene and CO for SCR reaction were chosen because their concentration changed monotonically with reaction time. In thermal reduction of NO<sub>2</sub>, the initial reaction rates increased with temperature. Propylene-SCR of NO<sub>2</sub> did not occur to any great extent in nanocrystalline NaY zeolite at room temperature. In propylene-SCR of NO<sub>2</sub>, the initial reaction rates at 373 K were approximately the same as those at 473 K. This reveals a free radical behavior for the early stage of SCR reactions as the reaction rates are independent of temperature once a certain threshold temperature is reached in which the free radicals are formed. The high CO to CO<sub>2</sub> ratio in Table 3 also suggests a free radical pathway [7].

## 4. Discussion

### 4.1. Formation of NO in thermal reduction of NO<sub>2</sub>

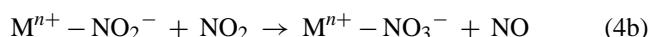
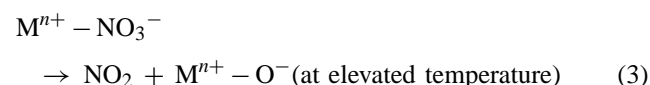
In earlier studies it was found that the adsorption of NO<sub>2</sub> on ion exchanged Y zeolite occurred preferentially via surface nitrates on exchangeable metal cation sites and partly on cationic EFAL [12]. A second pathway has been proposed involving the reaction between strongly adsorbed water and NO<sub>2</sub> [9,11]. Other studies indicate the possibility that nitrate is formed via two or more different mechanisms that populate different sites [7]. The disproportionation of NO<sub>2</sub> has been suggested to explain the formation of surface species and NO over CuZSM-5 [41]. Underwood and co-workers proposed a mechanism involving the formation of nitrite first followed by nitrate [37].

Based on the experimental observations, the formation of surface nitrate and nitrite in NaY zeolite can be best explained by reactions 1 and 2.



Reaction 1 is the minor path since only a trace amount of water is left in the zeolite after heating to 673 K under vacuum. However, adsorption of NO<sub>2</sub> happens preferentially via reaction 1 in the presence of water, as indicated by the formation of nitrite ( $1230 \text{ cm}^{-1}$ ) in the spectra shown in Fig. 4.

In this study, decomposition of NO<sub>2</sub> should involve the participation of NO<sub>2</sub> from the gas phase. An equilibrium might exist between surface NO<sub>x</sub><sup>-</sup> species and gaseous NO<sub>2</sub> (reaction 3). At elevated temperature, NO<sub>2</sub> was released from the NaY zeolite and reacted with surface cationic sites (reaction 4a) or nitrite (reaction 4b). M<sup>n+</sup> represents Na<sup>+</sup> or EFAL sites.



The small amount of N<sub>2</sub>O produced in thermal reduction of NO<sub>2</sub> might come from the disproportionation of NO [12,38,56]. Significant thermal reduction of NO to N<sub>2</sub>O was observed only at temperature above 573 K.

Notably, the concentration of NO reached a maximum at  $t = 150$  min and was constant thereafter (Fig. 5). Conversion of surface NO<sub>3</sub><sup>-</sup> species increased from 64% at 373 K to 90% at 473 K (Table 1). This means that some of the NO<sub>3</sub><sup>-</sup> species are more strongly adsorbed and less reactive. Two different reactivity classes of surface nitrates in zeolite Y have been observed in other studies [7].

### 4.2. Formation of NO and N<sub>2</sub>O in the adsorption of NO<sub>2</sub> and propylene mixture at room temperature

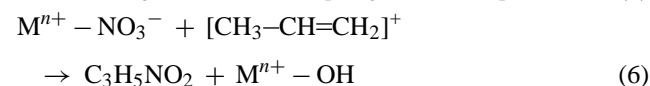
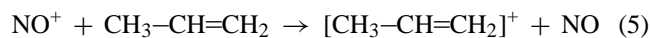
The concentration of NO and N<sub>2</sub>O upon adsorption of the NO<sub>2</sub> and propylene mixture (Fig. 10) was consistently higher than that after the adsorption of NO<sub>2</sub> alone (Fig. 5). Surface adsorbed NO and N<sub>2</sub>O<sub>3</sub> ( $1969$  and  $1943 \text{ cm}^{-1}$ , respectively) were observed upon exposure of the mixture to NaY zeolite (Fig. 7), but not in the adsorption of NO<sub>2</sub> alone (Fig. 4).

Although NO<sup>+</sup> was not observed in the adsorption of NO<sub>2</sub> and propylene mixture, it could play an important role due to its low thermal stability and high reactivity. Gerlach et al. studied the reactivity of NO<sup>+</sup> towards propylene over acidic Mordenite [18]. Their study demonstrated that oxime was produced in the reaction between NO<sup>+</sup> and propylene at 393 K and converted into nitrile at higher temperature. In this study, the disappearance of NO<sup>+</sup> by propylene adsorption was observed at room temperature. First the NaY zeolite was equilibrated with NO<sub>2</sub> at room temperature. Then propylene was introduced to NO<sub>2</sub> pre-adsorbed NaY zeolite. NO<sup>+</sup> vanished immediately upon the introduction of propylene. At the same time, surface adsorbed NO and N<sub>2</sub>O<sub>3</sub> are observed. Other new surface species observed in adsorption of NO<sub>2</sub> and propylene mixture (Fig. 7) appear within 1 min after adsorp-



tion. The intensity of  $1407\text{ cm}^{-1}$  band characterizing surface  $\text{Na}^+$ -nitrates didn't change significantly. This implies that at  $T=298\text{ K}$  surface  $\text{Na}^+$ -nitrate is inactive toward reaction with adsorbed propylene [7].

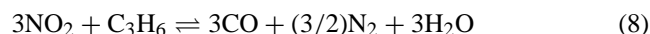
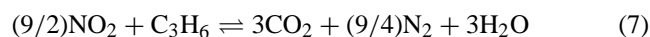
Thus it is suggested from the data that  $\text{NO}^+$  and  $\text{NO}_3^-$  on EFAL produced upon adsorption of  $\text{NO}_2$  (reaction 2) react readily with adsorbed propylene to form NO and organic nitro/nitrito compounds (reactions 5 and 6).



The high reactivity of the  $\alpha$ -H in propylene and the stabilization of allylic species by cations in zeolite Y could facilitate these two reactions [57,58]. Reaction 6 can lead to the generation of acidic hydroxyl groups. This is consistent with the appearance of a broad band at  $3562\text{ cm}^{-1}$  associated with hydroxyl groups on EFAL (Fig. 7). Oxime was then produced in the reaction between  $\text{NO}^+$  and adsorbed propylene in presence of the weak Bronsted acidic sites. It is also possible that organic nitro/nitrito compounds came from the direct reaction between adsorbed propylene and certain nitrate species, most likely those attached to EFAL sites populated on the external surface of the nanocrystalline NaY zeolite used in this study.

#### 4.3. Reaction stoichiometry in propylene-SCR of $\text{NO}_2$

In the absence of oxygen, the balanced reaction for complete reduction of  $\text{NO}_2$  by propylene can be written either as



assuming  $\text{CO}_2$  or  $\text{CO}$  as the only carbon-containing products, respectively.

As shown in Table 3, a high CO to  $\text{CO}_2$  ratio was observed at both 373 and 473 K. Therefore, it can be concluded that the majority of the propylene-SCR of  $\text{NO}_2$  in nanocrystalline NaY zeolite occurs via reaction 8 at low temperatures. The concentration of  $\text{CO}_2$  was much higher at 473 K than 373 K. This can be easily understood since higher temperature promotes decomposition of oxygenated species and the oxidation of CO to  $\text{CO}_2$ . The initial reaction rates for  $\text{NO}_2$  and CO at both 373 and 473 K are approximately three times that found for propylene (Table 4). Thus, the stoichiometry shown in reaction 8 is in agreement with the measured rate data.

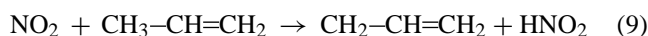
Water was also observed in the gas phase in propylene-SCR of  $\text{NO}_2$  at both 373 and 473 K (Fig. 9). However, surface adsorbed water was not present to any great extent in the zeolite after SCR reaction for 6 h. It is most likely that surface adsorbed water was consumed in the hydrolysis of surface species, such as organic nitrile.

It is difficult to write the balanced reaction for propylene-SCR of  $\text{NO}_2$  in the presence of excess oxygen because of the multiple reaction pathways involved and the complexities of these reactions. Complete oxidation of propylene by oxygen to  $\text{CO}_2$  and water does occur in nanocrystalline NaY zeolite at 473 K. This can be seen by the high  $\text{CO}_2$  to CO ratio (Table 3) and the existence of surface adsorbed water after SCR reaction for 6 h. As mentioned previously, NO reduction occurred very slowly once propylene was completely consumed. The low SCR reaction rate is possibly due to a combination of no propylene and the presence of surface adsorbed water. Although oxygen does decrease the zeolite deactivation by oxidizing carbonaceous deposits [6,59], overall it is detrimental to the propylene-SCR of  $\text{NO}_2$ .

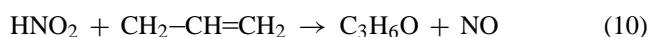
#### 4.4. A mechanism for propylene-SCR of $\text{NO}_2$ at low temperature

Several studies have focused on the mechanism for HC-SCR of  $\text{NO}_x$ . Most of them have suggested that isocyanate is an important intermediate. The most controversial and least understood aspect of the selective catalytic reduction of  $\text{NO}_2$  is the formation of the nitrogen-nitrogen bond which is necessary for the production of  $\text{N}_2$ . In the SCR reaction over Fe/ZSM-5, isotopic studies have shown that the nitrogen in  $\text{N}_2$  comes from both the gas phase  $\text{NO}_x$  and surface nitrogen-containing species [60]. Radical mechanisms involving azoxy or dinitroso species have been proposed to explain the formation of dinitrogen in zeolites containing transition metals [17,57]. Others have considered  $-\text{NH}$  complexes as the key intermediate [48]. Recently, Yeom et al. studied the reactions of acetaldehyde, acetic acid and nitromethane with  $\text{NO}_2$  on BaNa-Y zeolite [7]. Their study led to the conclusion that the formation of ammonium nitrite ( $\text{NH}_4\text{NO}_2$ ) is a crucial step for  $\text{DeNO}_x$  catalysis. They also suggested a parallel reaction channel involving free radicals to explain reaction pathways which result in a high CO to  $\text{CO}_2$  ratio [7].

Based on the observed kinetics and the discussion of the literature above, a mechanism involving free radicals appears to be the most plausible pathway for propylene-SCR of  $\text{NO}_2$  in nanocrystalline NaY zeolite. Thermal treatment is necessary for C–H bond dissociation in propylene [61]. At elevated temperature, the SCR reaction is initiated by the abstraction of H from adsorbed propylene to yield the allyl radical, according to reaction 9 [62,63].



The allylic radical can react with  $\text{HNO}_2$  to give oxygenated species and NO (reaction 10).



Upon thermal treatment, surface nitrogen containing compounds (organic nitro/nitrito species and oximes) adsorbed on EFAL sites are converted to nitrile or isocyanate. Acry-

lamide species can be produced via the hydrolysis of organic nitrile or isocyanate. The reaction between acrylamide and  $\text{HNO}_2$  (reaction 11) provides one possible pathway for the dinitrogen formation [64,65].



Another possible channel is the reaction between acrylamide and  $\text{N}_2\text{O}_3$  in the presence of water.

In propylene-SCR of  $\text{NO}_2$ , isocyanate radical ( $2317\text{ cm}^{-1}$ ) and isocyanic acid ( $2272\text{ cm}^{-1}$ ) were generated as stable species containing one atom each of nitrogen, carbon and oxygen. Isocyanic acid adsorbed in nanocrystalline NaY zeolite very strongly and can be removed by heating to 573 K under vacuum. It was considered as the precursor of ammonia, which is essential for the formation of dinitrogen [7,66]. In our study, a minor pathway for nitrogen-nitrogen bond formation might involve the reactions of isocyanate radical and isocyanic acid as evidenced by the presence of these species in the FT-IR spectra [51].

## 5. Conclusions

Catalytic reduction of  $\text{NO}_2$  in nanocrystalline NaY zeolite was investigated using in situ transmission FT-IR spectroscopy.  $\text{NO}_2$  was stored in the NaY zeolite as nitrate and nitrite. Because of the relatively high external surface area of the nanocrystalline zeolite, there was considerable adsorption on the EFAL sites. Thermal reduction of  $\text{NO}_2$  showed high selectivity to NO in the temperature range studied.

In the absence of oxygen, the selective catalytic reduction of  $\text{NO}_2$  with propylene at low temperature ( $T \leq 473\text{ K}$ ) resulted in complete reduction of  $\text{NO}_2$  to  $\text{N}_2$  and  $\text{O}_2$  in nanocrystalline NaY zeolite. Upon adsorption of propylene and  $\text{NO}_2$  mixtures at room temperature, surface organic nitro/nitrite compounds were produced together with other surface species. Isocyanate and nitrile species formed on EFAL sites are found to be important intermediates. Based on kinetic studies, a pathway involving radical reactions appeared to be the most plausible mechanism for the complete reduction of  $\text{NO}_2$ . In the proposed mechanism, complete reduction of  $\text{NO}_2$  was initiated by H abstraction from propylene. The resulting radical,  $\text{HNO}_2$ , then continues on to form  $\text{N}_2$ .

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## References

- [1] G. Delahay, B. Coq, Catal. Sci. Ser. 3 (2002) 345.
- [2] V.H. Grassian, Int. Rev. Phys. Chem. 20 (2001) 467.
- [3] S. Bhattacharyya, R.K. Das, Int. J. Energy Res. 23 (1999) 351.
- [4] R. Burch, J.P. Breen, F.C. Meunier, Appl. Catal. B: Environ. 39 (2002) 283.
- [5] Y. Traa, B. Burger, J. Weitkamp, Micro. Meso. Mater. 30 (1999) 3.
- [6] M. Shelef, Chem. Rev. 95 (1995) 209.
- [7] Y.H. Yeom, B. Wen, W.M.H. Sachtler, E. Weitz, J. Phys. Chem. B 108 (2004) 5386.
- [8] B. Wen, Y.H. Yeom, E. Weitz, W.M.H. Sachtler, Appl. Catal. B: Environ. 48 (2004) 125.
- [9] J. Szanyi, J.H. Kwak, C.H.F. Peden, J. Phys. Chem. B 108 (2004) 3746.
- [10] S.J. Schmiege, B.K. Cho, S.H. Oh, Appl. Catal. B: Environ. 49 (2004) 113.
- [11] J. Szanyi, J.H. Kwak, R.A. Moline, C.H.F. Peden, Phys. Chem. Chem. Phys. 5 (2003) 4045.
- [12] C. Sedlmair, B. Gil, K. Seshan, A. Jentys, J.A. Lercher, Phys. Chem. Chem. Phys. 5 (2003) 1897.
- [13] A. Sultana, R. Loenders, O. Monticelli, C. Kirschhock, P.A. Jacobs, J.A. Martens, Angew. Chem. Int. Ed. 39 (2000) 2934.
- [14] O. Monticelli, R. Loenders, P.A. Jacobs, J.A. Martens, Appl. Catal. B: Environ. 21 (1999) 215.
- [15] R. Brosius, J.A. Martens, Top. Catal. 28 (2004) 119.
- [16] V.A. Sadykov, V.V. Lunin, V.A. Matyshak, E.A. Paukshtis, A.Y. Rozovskii, N.N. Bulgakov, J.R.H. Ross, Kinet. Catal. 44 (2003) 379.
- [17] R.H.H. Smits, Y. Iwasawa, Appl. Catal. B: Environ. L6 (1995) 201.
- [18] T. Gerlach, F.W. Schutze, M. Baerns, J. Catal. 185 (1999) 131.
- [19] Y. Yu, H. He, Q. Feng, H. Gao, X. Yang, Appl. Catal. B: Environ. 49 (2004) 159.
- [20] M. Haneda, Y. Kintaichi, M. Inaba, H. Hamada, Catal. Today 42 (1998) 127.
- [21] T. Tanaka, T. Okuhara, M. Misono, Appl. Catal. B: Environ. 4 (1994) L1.
- [22] A. Satsuma, T. Enjoji, K. Shimizu, K. Sato, H. Yoshida, T. Hattori, J. Chem. Soc., Faraday Trans. 94 (1998) 301.
- [23] W. Song, G. Li, V.H. Grassian, S.C. Larsen, Environ. Sci. Tech. (2004), in press.
- [24] S.C. Larsen, V.H. Grassian, in: J.A. Schwarz, C.I. Contescu, K. Putyera (Eds.), Encyclopedia of Nanoscience and Nanotechnology, Marcel Dekker Publishing Co., NY, 2004, 1137.
- [25] Q. Li, D. Creaser, J. Sterte, Chem. Mater. 14 (2002) 1319.
- [26] W. Song, R.E. Justice, C.A. Jones, V.H. Grassian, S.C. Larsen, Langmuir 20 (2004) 4696.
- [27] G. Li, M. Xu, S.C. Larsen, V.H. Grassian, J. Mol. Catal. A: Chem. 194 (2003) 169.
- [28] H.G. Karge, Micro. Meso. Mater. 22 (1998) 547.
- [29] S. Khabtoui, T. Chevreau, J.C. Lavalley, Micro. Mater. 3 (1994) 133.
- [30] P.O. Fritz, J.H. Lunsford, J. Catal. 118 (1989) 85.
- [31] Y. Xiang, S.C. Larsen, V.H. Grassian, J. Am. Chem. Soc. 121 (1999) 5063.
- [32] F. Thibault-Starzyk, B. Gil, S. Aiello, T. Chevreau, J. Gilson, Micro. Meso. Mater. 67 (2004) 107.
- [33] M.R. Basila, T.R. Kantner, K.H. Rhee, J. Phys. Chem. 68 (1964) 3197.
- [34] A.L. Goodman, E.T. Bernard, V.H. Grassian, J. Phys. Chem. A 105 (2001) 6443.
- [35] K.I. Hadjiivanov, Catal. Rev. Sci. Eng. 42 (2000) 71.
- [36] A.L. Goodman, T.M. Miller, V.H. Grassian, J. Vacuum Sci. Tech. A 16 (1998) 2585.
- [37] A.L. Goodman, G.M. Underwood, V.H. Grassian, J. Phys. Chem. A 103 (1999) 7217.
- [38] C.C. Chao, J.H. Lunsford, J. Am. Chem. Soc. 93 (1971) 71.
- [39] C.C. Chao, J.H. Lunsford, J. Am. Chem. Soc. 93 (1971) 6794.

- [40] K. Hadjiivanov, J. Saussey, J.L. Freysz, J.C. Lavalley, *Catal. Lett.* 52 (1998) 103.
- [41] K. Hadjiivanov, D. Klissurski, G. Ramis, G. Busca, *Appl. Catal. B: Environ.* 7 (1996) 251.
- [42] S.V. Gerei, E.V. Rozhkova, Y.B. Gorokhovatskii, *J. Catal.* 28 (1973) 341.
- [43] B.A. Morrow, I.A. Cody, *J. Chem. Soc., Faraday Trans. 1* (71) (1975) 1021.
- [44] F. Solymosi, T.J. Bansagi, *J. Catal.* 156 (1995) 75.
- [45] V.H. Grassian, *J. Phys. Chem. A* 106 (2002) 860.
- [46] J.M. Garcia-Cortes, J. Perez-Ramirez, J.N. Rouzaud, A.R. Vaccaro, M.J. Illan-Gomez, C. Salinas-Martinez De Lecea, *J. Catal.* 218 (2003) 111.
- [47] A.L. Smith, *Applied Infrared Spectroscopy: Fundamentals, Techniques, and Analytical Problem Solving*, 1979.
- [48] M. Haneda, N. Bion, M. Daturi, J. Saussey, J. Lavalley, D. Duprez, H. Hamada, *J. Catal.* 206 (2002) 114.
- [49] Y. Ukisu, S. Sato, A. Abe, K. Yoshida, *Appl. Catal. B: Environ.* 2 (1993) 147.
- [50] G.R. Bamwenda, A. Ogata, A. Obuchi, J. Oi, K. Mizuno, J. Skrzypek, *Appl. Catal. B: Environ.* 6 (1995) 311.
- [51] W. Schiesser, H. Vinek, A. Jentys, *Appl. Catal. B: Environ.* 33 (2001) 263.
- [52] S. Sumiya, H. He, A. Abe, N. Takezawa, K. Yoshida, *J. Chem. Soc., Faraday Trans.* 94 (1998) 2217.
- [53] K. Hadjiivanov, L. Dimitrov, *Micro. Meso. Mater.* 27 (1999) 49.
- [54] I. Kiricsi, H. Foerster, G. Tasi, *J. Mol. Catal.* 65 (1991) L29.
- [55] T.E. Hoost, K.A. Laframboise, K. Otto, *Appl. Catal. B: Environ.* 7 (1995) 79.
- [56] T. Weingand, S. Kuba, K. Hadjiivanov, H. Knoezinger, *J. Catal.* 209 (2002) 539.
- [57] N.W. Hayes, R.W. Joyner, E.S. Shpiro, *Appl. Catal. B: Environ.* 8 (1996) 343.
- [58] T. Beutel, B. Adelman, W.M.H. Sachtler, *Catal. Lett.* 37 (1996) 125.
- [59] J.L. d'Itri, W.M.H. Sachtler, *Appl. Catal. B: Environ.* 2 (1993) L7.
- [60] H.Y. Chen, T. Voskoboinikov, W.M.H. Sachtler, *J. Catal.* 186 (1999) 91.
- [61] E. Finocchio, G. Busca, V. Lorenzelli, R.J. Willey, *J. Catal.* 151 (1995) 204.
- [62] J. Vassallo, E. Miro, J. Petunchi, *Appl. Catal. B: Environ.* 7 (1995) 65.
- [63] A.D. Cowan, R. Duempelmann, N.W. Cant, *J. Catal.* 151 (1995) 356.
- [64] P.A.S. Smith, *The Organic Chemistry of Open-Chain Nitrogen Compounds*, vol. I, 1965.
- [65] H.Y. Chen, T. Voskoboinikov, W.M.H. Sachtler, *J. Catal.* 180 (1998) 171.
- [66] N.W. Cant, D.C. Chambers, A.D. Cowan, I.O. Liu, A. Satsuma, *Top. Catal.* 10 (2000) 13.